State of Washington Utilities and Transportation Commission

INSPECTION REPORT FOR LIQUIFIED PETROLEUM GAS FACILITIES

Inspection Information- General

Date of Inspection: 3/19/2018

UTC Inspector(s): Anthony Dorrough

Operator and OPID Walter Moa Inspection (Physical) Address:

162 Hwy 20

City:Port Townsend Zip: 98368 LAT: 48-116859 LONG: -122.760503 Mailing Address/Headquarters:

162 Hwy 20

City: Port Townsend State: WA Zip: 98368

INSPECTION REPORT FOR LIQUIFIED PETROLEUM GAS FACILITIES

Operator Representative

Company Representative(s):

Walter Moa Title:Owner

Phone No:Click here to enter text. Email:Click here to enter text.

INSPECTION REPORT FOR LIQUIFIED PETROLEUM GAS FACILITIES

System Configuration- General

Installation Date of Original System: 1986 (Paradise Propane)

Number of Services: 9 Number of Meters: 1

Is system located in a public place: (If Yes, describe): Yes, retail business frequented

by the public.

Total Storage Capacity in gallons: (Over 4,000 aggregate use NFPA 59 Code were applicable)

1000

Above Ground or Below Ground Tanks: Above Ground

Total Number: 1 Tank Cap. (gals.): 1000 Age of Tank: >30yrs Age of Pipe >30yrs Cathodic Protection on Tank/Line: None

Pipe Specification:

Steel: Unknown Steel Plastic: N/A Copper: N/A

Part 192	PART 191 REQUIREMENTS	S	II	N/AN/C
Part 192	Reporting Procedures	3		IN/AIN/C
.605(b)	Gathering data for incident reporting			
(4)	191.5 Each notice required by paragraph (a) shall be made by telephone.			
	191.9(a) 30-day follow up written report (Form 7100.2).			X
	191.9(b) Supplemental report (to 30-day follow up).			
	191.11 Distribution system annual report (7100.1-1) –No Incidents			
.605(a)	191.23 Reporting safety-related conditions (see 192.605(a) and (d). Each			
	operator shall prepare and follow a manual of written procedures for			
	conducting operation, maintenance and emergency responses. (d)			X
	these procedures must include instructions enabling persons to			
	recognize conditions that may be safety-related. –No Safety-related Conditions			
	PART 191 PROCEDURE REQUIREMENTS			
Section	Operation & Maintenance	S	U	N/AN/C
	Normal Operating Procedures			
.605(a)	.605(a) Plan reviewed and updated (1year/15 months).		X	
	.605(b)(3) Written procedures include making construction records, maps		X	
	and operating history available to appropriate personnel.		Λ	
	.605(b)(8) Periodically reviewing the work done by operator's personnel to			
	determine the effectiveness and adequacy of the procedures		X	
	used in normal operation and maintenance and modifying the		Λ	
	procedures when deficiencies are found.			
	.605(b)(9) Taking adequate precautions in excavated trenches to protect			
	personnel from the hazards of unsafe accumulations of vapor		X	
	or gas, and making available when needed at the excavation.			
	Tapping Pipelines Under Pressure	S	U	N/A N/C
.605(a)	.627 Hot taps must be made by a qualified crewNo Hot Taps			X
	Pipeline Purging Procedures	S	U	N/A N/C
	.629 Purging of pipelines must be done to prevent entrapment of an			
.605(a)	explosive mixture in the line.		X	
.003(a)	(a) Lines containing air must be properly purged.		Λ	
	(b) Lines containing gas must be properly purged.			
	Maintenance Procedures	S	U	N/A N/C
	.703(b) Each segment of pipeline that becomes unsafe must be replaced,		X	
.605(a)	repaired or removed from service.		Λ	
.003(a)	.703(c) Hazardous leaks must be repaired promptly.	\perp	X	
	Patrolling Procedures	S	U	N/A N/C
6.8.3.10	.721(a) Patrolling when necessary.		X	
	.721(b) Maximum interval between patrols of mains (when patrolling is			X
	necessary)No Mains in Places or on Structures with Anticipated Movement			Λ

	Distribution System Leakage Survey Procedures	S	U	N/A	N/C
	.723(b)(1) Leakage surveys are required in business district at intervals not exceeding 15 months but at least once each calendar year.		X		
.605(b)	.723(b)(2) Leakage surveys are required outside business district at intervals not exceeding 5 years and for cathodically unprotected distribution lines at intervals not exceeding 3 years.		X		
	Line Marker Procedures	S	U	N/A	N/C
.605(b)	.707 Line markers installed and labeled as required.		X		
	Test Requirements For Reinstating Service Lines	S	U	N/A	N/C
.605(b)	.725(a) Reinstated service lines must be tested in the same manner as new service lines. –No services were reinstated			X	
1000(13)	.725(b) A service line that is temporarily disconnected must be tested from the point of disconnection. – No services temporarily disconnected			X	
	Abandonment or Deactivation of Facilities Procedures	S	U	N/A	N/C
.605(b)	.727 The operator disconnects both ends, purges, and seals each end before abandonment or a period of deactivation where the pipeline is not being maintained.		X		
	Prevention of Accidental Ignition Procedures	S	U	N/A	N/C
	.751 Reduce the hazard of fire or explosion by:		X		
COE(h)	(a) Removal of ignition sources in presence of gas and provision of fire extinguisher.		X		
.605(b)	(b) Prevent welding or cutting on pipeline containing combustible mixture.		X		
	(c) Post warning signs.		X		
	Corrosion Control Procedures	S	U	N/A	N/C
	.453 Corrosion control procedures are established for design/installation –PE Pipe Only			X	
.605(b)(2)	.455(a) Pipelines installed after July 31, 1971: the buried segments are externally coated and cathodically protected within one year. –PE Pipe Only			X	
	.457(b) Cathodic protection is provided in areas of active corrosion on existing bare or ineffectively coated pipelines. –PE Pipe Only			X	
	.459 Examination of buried pipeline when exposed. –PE Pipe Only			X	
	.463 Cathodic protection level according to Appendix D criteria. –PE Pipe Only			X	<u> </u>
	.465(a) Pipe-to-soil monitoring (Annually/15 months). –PE Pipe Only .465(c) Interference bond monitoring (as required with rectifiers) –PE Pipe Only			X	
	.467 Electrical Isolation (including casings when applicable). – PE Pipe Only			X	
.605(b)	.471 Test lead maintenance. –PE Pipe Only			X	
	.473 Interference currents. –PE Pipe Only			X	
	.481 Atmospheric corrosion control monitoring (3 year).		X		
	.483 Remedial measures (general). –PE Pipe Only			X	
	.487 Remedial measures (distribution lines other than cast iron or ductile iron). –PE Pipe Only			X	

Section	Emergency Procedures	S	U	N/A	N/C
	(a)(1) Receiving, identifying, and classifying notices of events which require		X		
	immediate response by the operator. (a)(2) Establish and maintain communication with appropriate public				
	officials regarding possible emergency.		X		
	(a)(3) Prompt response to each of the following emergencies: (i) Gas detected inside a building.				
	(i) Gas detected inside a building.		X		
	(iii) Explosion near a pipeline.				
	(iv)Natural disaster. (a)(4) Availability of personnel, equipment, tools, & material required at the				
	scene of each type of emergency.		X		
	(a)(5) Actions directed towards protecting people first, then property.		X		
	(a)(6) Emergency shutdown or pressure reduction to minimize hazards to life or property.		X		
	(a)(7) Making safe any actual or potential hazard to life or property.		X		
.615	(a)(8) Notifying appropriate public officials required at the emergency scene & coordinating planned and actual responses with these officials.		X		
	(a)(9) Instructions for restoring service outages after the emergency has been rendered safe.		X		
	(a)(10) Investigating accidents and failures as soon as possible after the emergency.		X		
	(b)(1) Furnishing applicable portions of the emergency plan to supervisory personnel who are responsible for emergency action.		X		
	(b)(2) Training appropriate employees as to the requirements of the emergency plan and verifying effectiveness of training.		X		
	(b)(3) Reviewing activities following emergencies to determine if the procedures were effective.		X		
	(b)(3)(c)				
	Establish and maintain liaison with appropriate public officials, such that both the operator and public officials are aware of each other's		X		
	resources & capabilities in dealing with gas emergencies.				
Section	Public Education Procedures	S	U	N/A	N/C
COE/-)	.616 Establishing a continuing educational program (in English & other		* 7		
.605(a)	pertinent languages) to better inform the public in how to recognize & report potential gas pipeline emergencies.		X		
Section	Failure Investigation Procedures	S	U	N/A	N/C
.617	Analyzing accidents & failures including laboratory analysis where		X		
	appropriate to determine cause & prevention of recurrence.		4.		
Section	Tanks - NFPA 58 REQUIREMENTS*	s	U	N/A	N/C

5.72.8 o Pressure (piskg) at which valve is set to start to leak Rated relieving capacity in from of air at 60 °F and 14.7 psia o Manufacturer's name and catalog number Short of valves shall not be installed between the container and pressure relief device. 5.72.10 Pressure relief devices shall be designed to minimize tampering. Containers up to 4000 gal water capacity shall comply with Table 5.7.7.1, Containers up to 4000 gal water capacity shall comply with Table 5.7.7.1, Outside If facility has tank(s) greater than 2000 gal water capacity AND is a bulk or industrial plant, inspector to review the cellity for compliance with 5.7.7.3, below. B) For containers over 4000 gal water capacity or meets description in Note above, must comply with: 1) For vapor and liquid withdrawal openings: 2. Postive shut off valve located as close to the tank as possible. 3. An internal valve with an integral excess flow valve or excess flow protection.— Tank 4,000 Gal 2) For vapor and liquid intel openings: 3. An opetive shut off valve in combination with either a backflow check valve or excess flow valve. 4. An internal valve with an integral excess flow valve or excess flow protection. 3) Other container appurtenances: 3. An internal spring-type, flush-type full internal, or external pressure relief valve (See Annex A), 4. Fixed liquid level gauge. 4. Prossure gauge. 5. Float gauge, noter yague, or slip tube gauge. 6. Prossure sauge. 6. Prossu		B) Pressure relief valves shall be marked accordingly:		
O Manufacturer's name and catalog number Str.2.9 Pressure relief devices shall be designed to minimize tampeting. Containers up to 4000 gal water capacity shall comply with Table 5.7.7.1. Column 5. Str.7.1 Note if facility has tank(s) greater than 2000 gal water capacity AND is a bulk or notustrial plant. Inspector to review facility for compliance with 5.7.7.3, below. B) For containers over 4000 gal water capacity or meets description in Note above, must comply with an integral excess flow valve or excess flow protection.—I ank 4.0.00 Gal 2) For vapor and liquid withdrawal openings: a. A positive shut-off valve located as close to the tank as possible. b. An internal valve with an integral excess flow valve or excess flow protection.—I ank 4.0.00 Gal 2) For vapor and liquid inlet openings: a. A positive shut-off valve in combination with either a backflow check valve or excess flow valve. b. An internal valve with an integral excess flow valve or excess flow protection. 3) Other container appurtenances: a. An internal spring-type, flush-type full internal, or external pressure relief valve (See Annex A). b. Fixed liquid level gauge. c. Florat gauge, rotary gauge, or slip tube gauge. d. Pressure gauge. e. Temperature gauge. Above ground tanks positioned no closer than 3 feet apart up to 2,000 gal, 5 feet apart 2,001 gallons or more. 6.3.3 bulldings.—Tank K-501 Gal Underground tanks of 2,000 gallons to 30,000 gallons are position at a minimum of 10 feet away from bulkings.—Tank K-501 Gal Underground tanks of 2,000 gallons to 30,000 gallons are position at a minimum of 10 feet away from bulkings.—Tank K-501 Gal Underground tanks of 2,000 gallons to 30,000 gallons are position at a minimum of 10 feet away from bulkings.—Tank K-501 Gal Underground tanks of 2,000 gallons to 30,000 gallons are position at a minimum of 10 feet away from bulkings.—Tank K-501 Gal Underground tanks of 2,000 gallons to 30,000 gallons are position at a minimum of 10 feet away from bulkings.—Tank shall be cortened so that their t	5.7.2.8		X	
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(Continued)				

	Cylinders shall be installed only aboveground and shall be set upon a firm foundation or otherwise be				
6.6.2.1	firmly secured. The cylinder shall not be in contact with the soil.	X			
6.6.6.1	If subject to loading from vehicles, there is at least eighteen inches of cover (for a non-interchangeable tank or, if the tank is an interchangeable tank, then no more than twelve inches of cover) and protected from vehicle traffic. Note: This item to be addressed on case by case basis. See items 6.6.6.1 (A) to (L) – Not Subject To Loading From Vehicles			X	
6.6.6.1(B)	The tank housing, piping, etc. in the above scenario is protected against traffic. – Not Subject To Loading From Vehicles			X	
6.6.6.1(D)	The tank, housing, piping, etc. is protected against vehicles.	X			
6.6.6.2(1)	Partially underground, unmounded ASME containers shall be protected against corrosion. –No Partially Underground Containers			X	
6.7.2.4	Rain caps or other means shall be provided to minimize the possibility of the entrance of water or other extraneous matter into the relief device or any discharge piping. Provisions shall be made for drainage where the accumulation of water is anticipated.	X			
6.7.2.6	The design of the pressure relief valve drain opening shall provide the following: (1) protection of the container against flame impingement resulting from ignited product escaping from the drain opening (2) direction of the pressure relief valve drain opening so that adjacent container(s), piping, or equipment are not subject to flame impingement.	X			
Section	Indirect-Fired & Electric Vaporizers - NFPA 58 REQUIREMENTS	S	U	N/A	N/C
6.19.2.1	Vaporizers installed in a building must comply with section 10.2 or 10.3. – No Vaporizers			X	
6.19.2.2	The building or structure shall not have any unprotected drains to sewer or sump pits. — No Vaporizers			X	
6.19.2.3	Pressure relief valves must be piped to the outside. – No Vaporizers			X	
6.19.2.4	If the heat source is gas-fired and located within 15 feet, see direct-fired vaporizers for requirements (6.19.3). — No Vaporizers			X	
6.19.2.6	If gas-fired heat source, it must have an automatic safety device. – No Vaporizers			X	
Section	Direct-Fired Vaporizers- NFPA 58 REQUIREMENTS	S	U	N/A	N/C
6.19.3.1	If vaporizer is in a building it must be built according to Chapter 10. – No Vaporizers			X	
6.19.3.2	Drains or sump pump cannot be shared with another structure. – No Vaporizers			X	
6.19.3.3	Pressure relief valve must be piped to the outside. – No Vaporizers			X	
6.19.3.5	A manual shutoff shall be installed in each connection of the container that is supplying the vaporizer. – No Vaporizers			X	
6.19.3.6	For direct-fired vaporizers see section 6.19.3.6 and 6.19.4.5: • Vaporizer is 10 feet from container; • Vaporizer is 15 feet from container shutoffs;			X	
0.13.3.0	 Vaporizer is 15 feet from the point of transfer (if transfer is within 15 ft, burner and pilot must be shut off when transferring liquid) Vaporizer is 25 feet from nearest building or property line. – No Vaporizers 			A	
6.19.6.1	If electrically heated, all electrical equipment must be Class 1, Group D. (Treat as an indirect-fired vaporizer) – No Vaporizers			X	
6.19.6.2	If not electrically heated, treat as direct-fired. – No Vaporizers			X	

Inspector Comments and Sketch of System: